

THE KAVERY ENGINEERING COLLEGE
(An Autonomous Institution)

BE/B.TECH DEGREE END SEMESTER THEORY EXAMINATIONS, NOV /DEC 2024

Sixth Semester

Chemical Engineering

CH3601 - CHEMICAL REACTION ENGINEERING- I

Regulations - 2021

Duration : 3 Hrs

Maximum : 100 Marks

PART - A (ANSWER ALL QUESTIONS) (Marks 10*2=20)

<i>Q.No</i>	<i>Questions</i>	<i>BLT</i>	<i>CO</i>	<i>Marks</i>
1.	Distinguish between homogeneous and heterogeneous reactions.	RE	1	2
2.	What is elementary reaction and non-elementary reactions?	UN	1	2
3.	Write the design equation for CSTR and PFR?	RE	2	2
4.	Give the basis on which chemical reactions and reactors are classified.	UN	2	2
5.	Write the classification of chemical reactors based on the method of operation and the number of phases in the reaction mixture.	RE	3	2
6.	Distinguish between holding time and space time for flow reactors.	UN	3	2
7.	What do you mean by optimum recycle operation?	UN	4	2
8.	Define optimum temperature progression?	UN	4	2
9.	Differentiate space time and mean holding time.	UN	5	2
10.	What are the factors responsible for deviations from ideal plug flow in a tubular reactor?	UN	5	2

PART - B (ANSWER ALL QUESTIONS) (Marks 5*13 = 65)

<i>Q.No</i>	<i>Questions</i>	<i>BLT</i>	<i>CO</i>	<i>Marks</i>
11.	a At 500 K the rate of a bimolecular reaction is ten times the rate at 400 K. Find the activation energy for this reaction (i). From Arrhenius law (ii). From Collision theory (iii). What is the % difference in rate of reaction at 600 K predicted by these two methods?	UN	1	13
	Or			
	b Explain the kinetic models for non-elementary reactions.	UN	1	13
12.	a Derive the performance equation for Plug flow reactor with schematic representation and write the assumptions made.	AP	2	13
	Or			
	b Derive the performance equation for steady state continuous stirred tank reactor with schematic representation and write the assumptions made.	AP	2	13

13. a Liquid reactant A produces R and S by the following reactions: AP 3 13
- $$A \rightarrow R, \quad r_R = k_1 CA^2, \quad k_1 = 0.4 \text{ m}^3/(\text{mol} \cdot \text{min})$$
- $$A \rightarrow S, \quad r_S = k_2 CA, \quad k_2 = 2 (\text{min})^{-1}$$
- A feed of aqueous A with $C_{A0} = 40 \text{ mol/m}^3$, enters a reactor, reacts to produce R and S, and a mixture of A, R and S leaves. Find C_R , C_S and τ for 90% conversion of A in a MFR.

Or

- b Reactant A in a liquid produces R and S by the following scheme: AP 3 13
- $$A \rightarrow R, A \rightarrow S$$
- Both these reactions are first order. A feed with $C_{A0} = 1$, $C_{R0} = 0$ and $C_{S0} = 0$, enters in two MFRs in series ($\tau_1 = 2 \text{ min}$; $\tau_2 = 5 \text{ min}$). The composition in the first reactor is $C_{A1} = 0.40$, $C_{R1} = 0.40$ and $C_{S1} = 0.20$. Find the composition leaving the second reactor.

14. a Explain irreversible first order reaction in series and derive the maximum concentration of intermediates and products. AN 4 13
- $$A \longrightarrow R \longrightarrow S$$
- with k_1 and k_2 are rate constants for two reactions respectively.

Or

- b Examine the effect of temperature and pressure on equilibrium conversion? AN 4 13

15. a i) Plot $C(t)$ and $E(t)$. AP 5 13
- (ii) Determine the fraction of material leaving the reactor that has spent time between 3 and 6 minutes in the reactor and the fraction of material leaving that has spent 7.75 and 8.25 minutes in the reactor.

t, min	0	1	2	3	4	5	6	7	8	9	10	12	14
E, min ⁻¹	0	0.02	0.10	0.16	0.20	0.16	0.12	0.08	0.06	0.44	0.03	0.012	0

Or

- b The concentration reading in the table represents a continuous response to a pulse input; AP 5 13

t, min	0	5	10	15	20	25	30	35
C, gm/lit	0	3	5	5	4	2	1	0

This vessel is used as a reactor for a liquid decomposing with rate $-r_A = k C_A$ & $k = 0.307 \text{ min}^{-1}$. Find the conversion expected in the reactor and compare it with the PFR

by

- (i) Direct use of Tracer curve.
(ii) Using Dispersion model.

*PART – C (Marks 1*15 = 15)*

<i>Q.No</i>		<i>Questions</i>	<i>BLT</i>	<i>CO</i>	<i>Marks</i>
16.	a	A homogenous liquid phase reaction $A \rightarrow R$, $-r_A = k C_A^2$, takes place with 50 % conversion in mixed flow reactor. i) What will be conversion if reactor is replaced by 6 times as large as the reactor, all other remaining unchanged? ii) What will be conversion if original reactor is replaced by PFR of same size?	AP	3	15
		Or			
	b	i) What are the factors affecting choice of reactors? Write its important significance of each reactor.	AP	3	10
		ii) Explain selectivity and reactivity in detail.	AP	3	5